

**TITLE 33--NAVIGATION AND
NAVIGABLE WATERS**

**CHAPTER I--COAST GUARD,
DEPARTMENT OF TRANSPORTATION
(CONTINUED)**

**PART 154--FACILITIES TRANSFERRING OIL OR
HAZARDOUS MATERIAL IN BULK**

Subpart E--Vapor Control Systems

§154.800 Applicability.

(a) Except as specified by paragraph (c) of this section, this subpart applies to:

(1) Each facility which collects vapors of crude oil, gasoline blends, or benzene emitted from vessel cargo tanks;

(2) A vessel which is not a tank vessel that has a vapor processing unit located on board for recovery, destruction, or dispersion of crude oil, gasoline blends, or benzene vapors from a tank vessel; and

(3) Certifying entities which review, inspect, test, and certify facility vapor control systems.

(b) A facility which collects vapors of flammable or combustible cargoes other than crude oil, gasoline blends, or benzene, must meet the requirements prescribed by the Commandant (G-MSO).

(c) A facility with an existing Coast Guard approved vapor control system which was operating prior to July 23, 1990 is subject only to §154.850 of this subpart as long as it receives cargo vapor only from the specific vessels for which it was approved.

(d) This subpart does not apply to the collection of vapors of liquefied flammable gases as defined in 46 CFR 30.10-39.

(e) When a facility vapor control system which receives cargo vapor from a vessel is connected to a facility vapor control system that serves tank storage areas and other refinery processes, the specific requirements of this subpart apply between the vessel vapor connection and the point where the vapor control system connects to the facility's main vapor control system.

§154.802 Definitions.

As used in this subpart:

Certifying entity means an individual or organization accepted by the Commandant (G-MSO) to review plans and calculations for vapor control system designs, and to conduct initial inspections and witness tests of vapor control system installations.

Existing vapor control system means a vapor control system which was operating prior to July 23, 1990.

Facility vapor connection means the point in a facility's vapor collection system where it connects to a vapor collection hose or the base of a vapor collection arm.

Inerted means the oxygen content of the vapor space in a tank vessel's cargo tank is reduced to 8 percent by volume or less in accordance with the inert gas requirements of 46 CFR 32.53 or 46 CFR 153.500.

Liquid knockout vessel means a device to separate liquid from vapor.

Maximum allowable transfer rate means the maximum volumetric rate at which a vessel may receive cargo or ballast.

New vapor control system means a vapor control system which is not an existing vapor control system.

Vapor balancing means the transfer of vapor displaced by incoming cargo from the tank of a vessel receiving cargo into a tank of the vessel or facility delivering cargo via a vapor collection system.

Vapor collection system means an arrangement of piping and hoses used to collect vapor emitted from a vessel's cargo tanks and transport the vapor to a vapor processing unit.

Vapor control system means an arrangement of piping and equipment used to control vapor emissions collected from a vessel, and includes the vapor collection system and the vapor processing unit.

Vapor destruction unit means a vapor processing unit that destroys cargo vapor by a means such as incineration.

Vapor dispersion system means a vapor processing unit which releases cargo

vapor to the atmosphere through a venting system not located on the vessel being loaded or ballasted.

Vapor processing unit means the components of a vapor control system that recovers, destroys, or disperses vapor collected from a vessel.

Vapor recovery unit means a vapor processing unit that recovers cargo vapor by a non-destructive means such as lean oil absorption, carbon bed adsorption, or refrigeration.

Vessel vapor connection means the point in a vessel's fixed vapor collection system where it connects to a vapor collection hose or arm.

§154.804 Review, certification, and initial inspection.

(a) A new vapor control system installation must be certified by a certifying entity as meeting the requirements of this subpart prior to operating.

(b) [Reserved]

(c) An existing vapor control system installation that has been Coast Guard approved for operation with specific vessels must be certified by a certifying entity prior to receiving vapors from other vessels.

(d) Plans and information submitted to the certifying entity must include a qualitative failure analysis. The analysis must demonstrate the following:

(1) The vapor control system is designed to permit the system to continuously operate safely when receiving cargo vapors from tankships and barges over the full range of transfer rates expected at the facility;

(2) The vapor control system is provided with the proper alarms and automatic control systems to prevent unsafe operation;

(3) The vapor control system is equipped with sufficient automatic or passive devices to minimize damage to personnel, property, and the environment if an accident were to occur; and

(4) If a quantitative failure analysis is also conducted, the level of safety attained is at least one order of magnitude greater

than that calculated for operating without a vapor control system.

NOTE: *The American Institute of Chemical Engineers* publication, "Guidelines for Hazard Evaluation Procedures" may be used as guidance when preparing a qualitative failure analysis. Military Standard MIL-STD-882B may be used as guidance when preparing a quantitative failure analysis.

(e) The certifying entity must conduct all initial inspections and witness all tests required to demonstrate that the facility:

(1) Conforms to certified plans and specifications;

(2) Meets the requirements of this subpart; and

(3) Is operating properly.

(f) Upon receipt of written certification from the certifying entity that a facility's vapor control system complies with the requirements of this part the COTP shall endorse the letter of adequacy required by §154.325 of this part to indicate that the facility is acceptable for collecting vapors of crude oil, gasoline blends, benzene, or any other vapors for which it is certified.

(g) Any design or configuration alteration involving a certified vapor control system must be reviewed by a certifying entity. After conducting any inspections and witnessing tests necessary to verify that the modified vapor control system meets the requirements of this subpart, the certifying entity must recertify the installation.

(h) Certifications issued in accordance with this section and a copy of the plans, calculations, and specifications for the vapor control system must be maintained at the facility.

(i) A certifying entity accepted under §154.806 of this subpart may not certify a facility vapor control system if it was involved in the design or installation of the system.

§154.806 Application for acceptance as a certifying entity.

(a) An individual or organization seeking acceptance as a certifying entity must apply in writing to the Commandant (G-MSO). Each application must be signed

and certified to be correct by the applicant or, if the applicant is an organization, by an authorized officer or official representative of the organization, and must include a letter of intent from a facility owner or operator to use the services of the individual or organization to certify a vapor control system installation. Any false statement or misrepresentation, or the knowing and willful concealment of a material fact may subject the applicant to prosecution under the provisions of 18 U.S.C. 1001, and denial or termination of acceptance as a certifying entity.

(b) The applicant must possess the following minimum qualifications, and be able to demonstrate these qualifications to the satisfaction of the Commandant (G-MSO):

(1) The ability to review and evaluate design drawings and failure analyses;

(2) A knowledge of the applicable regulations of this subpart, including the standards incorporated by reference in these regulations;

(3) The ability to monitor and evaluate test procedures and results;

(4) The ability to perform inspections and witness tests of bulk liquid cargo handling systems;

(5) That it is not controlled by an owner or operator of a vessel or facility engaged in controlling vapor emissions; and

(6) That it is not dependent upon Coast Guard acceptance under this section to remain in business.

(c) Each application for acceptance must contain the following:

(1) The name and address of the applicant, including subsidiaries and divisions if applicable;

(2) A statement that the applicant is not controlled by an owner or operator of a vessel or facility engaged in controlling vapor emissions, or a full disclosure of any ownership or controlling interest held by such owners or operators;

(3) A description of the experience and qualifications of the person(s) who would be reviewing or testing the systems;

(4) A statement that the person(s) who would be reviewing or testing the systems is/are familiar with the regulations in this subpart; and

(5) A statement that the Coast Guard may verify the information submitted in the application and may examine the person(s) who would be reviewing or testing the systems to determine their qualifications.

(d) The acceptance of a certifying entity may be terminated by the Commandant (G-MSO) if the entity fails to properly review, inspect, or test a system in accordance with this subpart.

NOTE: A list of entities accepted to certify facility vapor control system installations is available from the Commandant (G-MSO).

§154.808 Vapor control system, general.

(a) A vapor control system design and installation must eliminate potential overflow hazards, overpressure and vacuum hazards, and sources of ignition to the maximum practical extent. Each remaining hazard source which is not eliminated must be specifically addressed in the protection system design and operational requirements.

(b) Vapor collection system piping and fittings must be in accordance with ANSI B31.3 and designed for a maximum allowable working pressure of at least 150 psig. Valves and flanges must be in accordance with ANSI B16.5 or B16.24, 150 pound class.

(c) All electrical equipment used in a vapor control system must comply with NFPA 70.

(d) Any pressure, flow, or concentration indication required by this part must provide a remote indicator on the facility where the cargo transfer and vapor control systems are controlled.

(e) Any alarm condition specified in this part must activate an audible and visible alarm where the cargo transfer and vapor control systems are controlled.

(f) The vapor control system must be separated or insulated from external heat sources to limit vapor control system piping surface temperature to not more than 177 deg.C. (350 deg.F.) during normal operation.

(g) A means must be provided to eliminate any liquid condensate from the vapor collection system which carries over

from the vessel or condenses as a result of an enrichment process.

(h) If a liquid knockout vessel is installed it must have:

(1) A means to indicate the level of liquid in the device;

(2) A high liquid level sensor that activates an alarm; and

(3) A high high level sensor that closes the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart and shuts down any compressors or blowers prior to liquid carrying over from the vessel to the compressor or blower.

(i) Vapor collection piping must be electrically grounded and electrically continuous.

(j) If the facility handles inerted vapors of cargoes containing sulfur, provisions must be made to control heating from pyrophoric iron sulfide deposits in the vapor collection line.

§154.810 Vapor line connections.

(a) A remotely operated cargo vapor shutoff valve must be installed in the vapor collection line between the facility vapor connection and the nearest point where any inerting, enriching, or diluting gas is introduced into the vapor collection line or where a detonation arrester is fitted. The valve must:

(1) Close within thirty (30) seconds after detection of a shutdown condition by a component required by this subpart;

(2) Close automatically if the control signal is lost;

(3) Activate an alarm when a signal to shut down is received;

(4) Be capable of manual operation or manual activation;

(5) Have a local valve position indicator or be designed so that the valve position can be readily determined from the valve handle or valve stem position; and

(6) If the valve seat is fitted with resilient material, not allow appreciable leakage when the resilient material is damaged or destroyed.

(b) Except when a vapor collection arm is used, the last 1.0 meter (3.3 feet) of

vapor piping before the facility vapor connection must be:

(1) Painted red/yellow/red with:

(i) The red bands 0.1 meter (0.33 feet) wide, and

(ii) The middle yellow band 0.8 meter (2.64 feet) wide; and

(2) Labeled "VAPOR" in black letters at least 50 millimeters (2 inches) high.

(c) Each facility vapor connection flange must have a permanently attached 0.5 inch diameter stud at least 1.0 inch long projecting outward from the flange face. The stud must be located at the top of the flange, midway between bolt holes, and in line with the bolt hole pattern.

(d) Each hose used for transferring vapors must:

(1) Have a design burst pressure of at least 25 psig;

(2) Have a maximum allowable working pressure of at least 5 psig;

(3) Be capable of withstanding at least 2.0 psi vacuum without collapsing or constricting;

(4) Be electrically continuous with a maximum resistance of ten thousand (10,000) ohms;

(5) Have flanges with:

(i) A bolt hole arrangement complying with the requirements for 150 pound class ANSI B16.5 flanges, and

(ii) One or more 0.625 inch diameter holes in the flange located midway between bolt holes and in line with the bolt hole pattern;

(6) Be abrasion resistant and resistant to kinking; and

(7) Have the last 1.0 meter (3.3 feet) of each end of the vapor hose marked in accordance with paragraph (b) of this section.

(e) Vapor hose handling equipment must be provided with hose saddles which provide adequate support to prevent kinking or collapse of hoses.

(f) Fixed vapor collection arms must:

(1) Meet the requirements of paragraphs (d)(1) through (d)(5) of this section;

(2) Have the last 1.0 meter (3.3 feet) of the arm marked in accordance with paragraph (b) of this section.

(g) The facility vapor connection must be electrically insulated from the vessel

vapor connection in accordance with section 6.10 of the OCIMF International Safety Guide for Oil Tankers and Terminals.

(h) A vapor collection system fitted with an enriching system that operates at a positive gauge pressure at the facility vapor connection must be fitted with:

(1) A manual isolation valve between each facility vapor connection and the remotely operated cargo vapor shutoff valve required by paragraph (a) of this section; and

(2) A means to prevent backflow of enriched vapor to the vessel's vapor collection system.

§154.812 Facility requirements for vessel liquid overflow protection.

(a) Each facility which receives cargo vapor from a tank barge which is fitted with overflow protection in accordance with 46 CFR 39.20-9(a) as its only means of overflow protection must provide a 120 volt, 20 amp explosion proof receptacle which meets:

(1) ANSI/NEMA WD6;

(2) NFPA 70, Articles 410-57 and 501-12; and

(3) 46 CFR 111.105-9.

(b) Each facility that receives cargo vapor from a tank barge fitted with an intrinsically safe cargo tank level sensor system complying with 46 CFR 39.20-9(b) as its only means of overflow protection must have an overflow control panel on the dock capable of powering and receiving an alarm and shutdown signal from the cargo tank level sensor system that:

(1) Closes the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart and activates the emergency shutdown system required by §154.550 of this part when:

(i) A tank overflow signal is received from the barge, or

(ii) Electrical continuity of the cargo tank level sensor system is lost;

(2) Activates an alarm which is audible and visible to barge personnel and facility personnel when a tank overflow signal, or an optional high level signal corresponding to a liquid level lower than the tank overflow sensor setting, is received from the barge;

(3) Has a means to electrically and mechanically test the alarms and automatic shutdown systems prior to transferring cargo to or ballasting the tank barge;

(4) Has suitable means, such as approved intrinsic safety barriers able to accept passive devices, to ensure that the overflow and optional alarm circuits on the barge side of the overflow control panel, including cabling, normally closed switches, and pin and sleeve connectors, are intrinsically safe;

(5) Is labeled with the maximum allowable inductance and capacitance to be connected to the panel, as specified by the equipment manufacturer; and

(6) Has a female connecting plug for the tank barge level sensor system with a 5 wire, 16 amp connector body meeting IEC 309-1/309-2 which is:

(i) Configured with pins S2 and R1 for the tank overflow sensor circuit, pin G connected to the cabling shield, and pins N and T3 reserved for an optional high level alarm connection;

(ii) Labeled "Connector for Barge Overflow Control System"; and

(iii) Connected to the overflow control panel by a shielded flexible cable.

§154.814 Facility requirements for vessel vapor overpressure and vacuum protection.

(a) A facility's vapor collection system must have the capacity for collecting cargo vapor at a rate of not less than 1.25 times the facility's maximum liquid transfer rate for cargo for which vapor collection is required plus any inerting, diluting, or enriching gas which may be added to the system, unless the vapor growth for turbulent loading of the most volatile liquid handled by the facility is less than 25 percent.

(b) A facility vapor collection system must maintain the pressure in a vessel's cargo tanks between 80 percent of the highest setting of any of the vessel's vacuum relief valves and 80 percent of the lowest setting of any of the vessel's pressure relief valves for a non-inerted tank

vessel, and between 0.2 psig and 80 percent of the lowest setting of any of the vessel's pressure relief valves for an inerted tank vessel. The system must be capable of maintaining the pressure in the vessel's cargo tanks within this range at any cargo transfer rate less than or equal to the maximum transfer rate determined at the pre-transfer conference required by § 156.120(w) of this chapter.

(c) The pressure measured at the facility vapor connection must be corrected for pressure drops across the vessel's vapor collection system and the vapor collection hose or arm.

(d) A pressure sensing device must be provided which activates an alarm when the pressure at the facility vapor connection exceeds either the pressure corresponding to the upper pressure determined in paragraph (b) of this section or a lower pressure agreed upon at the pre-transfer conference required by § 156.120(w) of this chapter.

(e) A pressure sensing device must be provided which activates an alarm when the pressure at the facility vapor connection falls below either the pressure corresponding to the lower pressure determined in paragraph (b) of this section or a higher pressure agreed upon at the pre-transfer conference required by § 156.120(w) of this chapter.

(f) A pressure sensing device must be provided which activates the emergency shutdown system required by §154.550 of this part and closes the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the pressure at the facility vapor connection exceeds 2.0 psi, or a lower pressure agreed upon at the pre-transfer conference required by §156.120(w) of this chapter. The sensing device must be independent of the device used to activate the alarm required by paragraph (d) of this section.

(g) A pressure sensing device must be provided which closes the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the vacuum at the facility vapor connection is more than 1.0 psi, or a lesser vacuum set at the pre-transfer conference

required by §156.120(w) of this chapter. The sensing device must be independent of the device used to activate the alarm required by paragraph (e) of this section.

(h) The pressure sensing devices required by paragraphs (d) and (f) of this section must be located in the vapor collection line between the facility vapor connection and the manual isolation valve, if required by §154.810(h) of this subpart, unless an interlock is provided which prevents operation of the system when the isolation valve is closed.

(i) A pressure indicating device must be provided which indicates the pressure in the vapor collection line.

(j) If a compressor, blower, or eductor capable of drawing more than 1.0 psi vacuum is used to draw vapor from the vessel, a vacuum relief valve must be installed in the vapor collection line between the compressor, blower, or eductor and the facility vapor connection, which:

(1) Relieves at a pressure such that the pressure in the vapor collection system at the facility vapor connection does not exceed 1.0 psi vacuum;

(2) Has a relieving capacity equal to or greater than the capacity of the compressor, blower, or eductor;

(3) Has a flame screen fitted at the vacuum relief opening; and

(4) Has been tested for relieving capacity in accordance with paragraph 1.5.1.3 of API 2000 with a flame screen fitted.

(k) When a facility collects cargo vapor through an undersea pipeline from a vessel moored offshore, the vacuum relief valve may be set at a vacuum greater than 1.0 psi vacuum provided the pressure controls take into account the pressure drop across the vessel's vapor collection system, any vapor collection hoses, and the undersea pipeline as a function of the actual transfer rate.

(l) If the pressure in the vapor collection system can exceed 2.0 psig due to a malfunction in an inerting, enriching, or diluting system a pressure relief valve must:

(1) Be installed between the point where inerting, enriching, or diluting gas is

introduced into the vapor collection system and the facility vapor connection;

(2) Relieve at a pressure such that the pressure in the vapor collection system at the facility vapor connection does not exceed 2.0 psig;

(3) Have a relieving capacity equal to or greater than the maximum capacity of the facility inerting, enriching, or diluting gas source;

(4) If not designed to insure a minimum vapor discharge velocity of 30 meters (98.4 ft.) per second, have a flame screen fitted at the discharge opening; and

(5) Have been tested for relieving capacity in accordance with paragraph 1.5.1.3 of API 2000.

(m) The relieving capacity test required by paragraph (l)(5) must be carried out with a flame screen fitted at the discharge opening if the pressure relief valve is not designed to insure a minimum vapor discharge velocity of 30 meters (98.4 ft.) per second.

§154.820 Fire, explosion, and detonation protection.

(a) A vapor control system with a single facility vapor connection that receives vapor only from a vessel with inerted cargo tanks and processes vapor with a vapor recovery unit must:

(1) Be capable of inerting the vapor collection line in accordance with §154.824(a) of this subpart prior to receiving vapors from the vessel;

(2) Have at least one oxygen analyzer that samples the vapor concentration continuously at a point not more than 6 meters (19.7 ft.) from the facility vapor connection; and

(3) Meet §154.824 (f)(1), (f)(2), (g), (h)(2), and (h)(3) of this subpart.

(b) A vapor control system with a single facility vapor connection that receives vapor only from a vessel with inerted cargo tanks and processes vapor with a vapor destruction unit must:

(1) Have a detonation arrester located not more than 6 meters (19.7 ft.) from the facility vapor connection; or

(2) Have an inerting system that meets the requirements of §154.824 of this subpart.

(c) A vapor control system with a single facility vapor connection that receives vapor from a vessel with cargo tanks that are not inerted and processes vapor with a vapor recovery unit must:

(1) Have a detonation arrester located not more than 6 meters (19.7 ft.) from the facility vapor connection; or

(2) Have an inerting, enriching, or diluting system that meets the requirements of §154.824 of this subpart.

(d) A vapor control system with a single facility vapor connection that receives vapor from a vessel with cargo tanks that are not inerted and processes the vapor with a vapor destruction unit must:

(1) Have a detonation arrester located not more than 6 meters (19.7 ft.) from the facility vapor connection; and

(2) Have an inerting, enriching, or diluting system that meets the requirements of §154.824 of this subpart.

(e) A vapor control system with multiple facility vapor connections that processes vapor with a vapor recovery unit must have a detonation arrester located not more than 6 meters (19.7 ft.) from each facility vapor connection.

(f) A vapor control system with multiple facility vapor connections that processes vapor with a vapor destruction unit must:

(1) Have a detonation arrester located not more than 6 meters (19.7 ft.) from each facility vapor connection; and

(2) Have an inerting, enriching, or diluting system that meets the requirements of §154.824 of this subpart.

(g) A vapor control system that uses a vapor balancing system in which cargo vapor from a vessel is transferred through the facility vapor collection system to facility storage tanks must:

(1) Have a detonation arrester located not more than 6 meters (19.7 ft.) from each facility vapor connection;

(2) Have a detonation arrester located within the storage tank containment area as close as practical to the vapor return connection of each facility storage tank; and

(3) Have facility storage tank high level alarm systems and facility storage tank overfill control systems arranged to prevent cargo from entering the vapor return line.

(h) Except for a discharge vent from a vapor destruction unit, each outlet of a vapor control system that vents to atmosphere and is not isolated with a pressure-vacuum relief valve must have a flame arrester located at the outlet.

§154.822 Detonation arresters, flame arresters, and flame screens.

(a) Each detonation arrester required by this part must:

(1) Be capable of arresting a detonation from either side of the device; and

(2) Be acceptable to the Commandant (G-MSO). A detonation arrester designed, built, and tested in accordance with appendix A of this part will be acceptable to the Commandant (G-MSO).

(b) Each flame arrester required by this part must be acceptable to the Commandant (G-MSO). A flame arrester designed, built, and tested in accordance with appendix B of this part will be acceptable to the Commandant (G-MSO).

(c) Each flame screen required by this part must be either a single screen of corrosion resistant wire of at least 30 by 30 mesh, or two screens, both of corrosion resistant wire, of at least 20 by 20 mesh, spaced not less than 12.7 millimeters (½ in.) or more than 38.1 millimeters (1½ in.) apart.

§154.824 Inerting, enriching, and diluting systems.

(a) A vapor control system which uses inerting, enriching, or diluting gas must be capable of inerting, enriching, or diluting the vapor collection line prior to receiving cargo vapor.

(b) Except as permitted by §154.820(a) of this subpart, a vapor control system which uses an inerting, enriching, or diluting system must be equipped with a gas injection and mixing arrangement located as close as practical but not more than 10 meters (32.8 ft.) from the facility vapor connection that ensures complete

mixing of the gases within 20 pipe diameters of the injection point;

(c) A vapor control system that uses an inerting or enriching system may not be operated at a vacuum after the injection point unless:

(1) There are no sleeve-type pipe couplings, vacuum relief valves, or other devices which could allow air into the vapor collection system downstream of the injection point; or

(2) An additional analyzer is used to monitor the downstream vapor concentration and a means is provided to inject additional inerting or enriching gas.

(d) A vapor control system that uses analyzers to control the amount of inerting, enriching, or diluting gas injected into the vapor collection line must be equipped with at least 2 analyzers. The analyzers must be connected so that:

(1) When oxygen analyzers are used, the higher oxygen concentration reading controls the inerting or enriching system and activates the alarm and automatic shutdown system required by paragraph (h), (j) or (k)(2) of this section;

(2) When hydrocarbon analyzers are used, the lower hydrocarbon concentration reading controls the enriching system and activates the alarm and automatic shutdown system required by paragraph (i) or (k)(1) of this section; and

(3) When hydrocarbon analyzers are used, the higher hydrocarbon concentration reading controls the diluting system and activates the alarm and automatic shutdown system required by paragraph (l) of this section.

(e) A vapor control system that uses volumetric measurements to control the amount of inerting, enriching, or diluting gas injected into the vapor collection line must be equipped with at least one analyzer to activate the alarms and automatic shutdown systems required by this section.

(f) Each oxygen or hydrocarbon analyzer required by this section must:

(1) Be installed in accordance with API Recommended Practice 550;

(2) Have a response time of not more than 30 seconds from the time the vapor is sampled; and

(3) Sample the vapor concentration continuously not more than 30 pipe diameters from the gas injection point.

(g) Oxygen analyzers which operate at elevated temperatures (i.e. zirconia oxide or thermomagnetic) must not be used.

(h) An inerting system must:

(1) Supply sufficient inert gas to the vapor stream to ensure that the oxygen concentration throughout the vapor collection system is maintained below 8.0 percent by volume;

(2) Activate an alarm when the oxygen concentration in the vapor collection line exceeds 8.0 percent by volume;

(3) Close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this part when the oxygen concentration in the vapor collection line exceeds 9.0 percent by volume; and

(4) If a combustion device is used to produce the inert gas, have a hydraulic seal and non-return valve between the combustion device and the vapor collection line.

(i) An enriching system must:

(1) Supply sufficient compatible hydrocarbon vapor to the vapor stream to ensure that the hydrocarbon concentration throughout the vapor collection system is maintained above 170 percent by volume of the upper flammable limit;

(2) Activate an alarm when the hydrocarbon concentration in the vapor collection line falls below 170 percent by volume of the upper flammable limit; and

(3) Close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the hydrocarbon concentration in the vapor collection line falls below 150 percent by volume of the upper flammable limit.

(j) Oxygen analyzers may be used in lieu of hydrocarbon analyzers in an enriching system at a facility that receives cargo vapor only from a vessel with non-inerted cargo tanks, provided that the analyzers:

(1) Activate an alarm when the oxygen concentration in the vapor collection line exceeds 15.5 percent by volume; and

(2) Close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the oxygen concentration in the vapor collection line exceeds 16.5 percent by volume.

(k) An enriching system may be used in a vapor collection system that receives cargo vapor from a vessel with inerted cargo tanks if:

(1) Hydrocarbon analyzers are used to comply with paragraph (i)(2) and (i)(3) of this section; or

(2) If oxygen analyzers are used, the analyzers activate an alarm when the oxygen concentration in the vapor collection line exceeds 8 percent by volume, and close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the oxygen concentration exceeds 9 percent by volume.

(l) An air dilution system must:

(1) Supply sufficient additional air to the vapor stream to ensure that the hydrocarbon concentration throughout the vapor collection system is maintained below 30 percent by volume of the lower flammable limit;

(2) Activate an alarm when the hydrocarbon concentration in the vapor collection line exceeds 30 percent by volume of the lower flammable limit; and

(3) Close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart when the hydrocarbon concentration in the vapor collection line exceeds 50 percent by volume of the lower flammable limit.

§154.826 Vapor compressors and blowers.

(a) Each inlet and outlet to a compressor or blower which handles vapor that has not been inerted, enriched, or diluted in accordance with §154.824 of this subpart must be fitted with:

(1) A detonation arrester;

(2) A flame arrester; or

(3) An explosion suppression system acceptable to the Commandant (G-MSO).

(b) If a reciprocating or screw-type compressor handles vapor in the vapor

collection system, it must be provided with indicators and audible and visible alarms to warn against the following conditions:

- (1) Excessive discharge gas temperature at each compressor chamber or cylinder;
- (2) Excessive cooling water temperature;
- (3) Excessive vibration;
- (4) Low lube oil level;
- (5) Low lube oil pressure; and
- (6) Excessive shaft bearing temperatures.

(c) If a liquid ring-type compressor handles vapor in the vapor collection system, it must be provided with indicators and audible and visible alarms to warn against the following conditions:

- (1) Low level of liquid sealing medium;
- (2) Lack of flow of liquid sealing medium;
- (3) Excessive temperature of the liquid sealing medium;
- (4) Low lube oil level;
- (5) Low lube oil pressure, if pressurized lubricating system; and
- (6) Excessive shaft bearing temperature.

(d) If a centrifugal compressor, fan, or lobe blower handles vapor in the vapor collection system, construction of the blades and/or housing must meet one of the following:

- (1) Blades or housing of nonmetallic construction;
- (2) Blades and housing of nonferrous material;
- (3) Blades and housing of corrosion resistant steel;
- (4) Ferrous blades and housing with one-half inch or more design tip clearance; or
- (5) Blades of aluminum or magnesium alloy and a ferrous housing with a nonferrous insert sleeve at the periphery of the impeller.

§154.828 Vapor recovery and vapor destruction units.

(a) The inlet to a vapor recovery unit which receives cargo vapor that has not been inerted, enriched, or diluted in accordance with §154.824 of this subpart must be fitted with one of the following:

- (1) A detonation arrester;
- (2) A flame arrester; or
- (3) An explosion suppression system acceptable to the Commandant (G-MSO).

(b) The inlet to a vapor destruction unit must:

- (1) Have a liquid seal; and
- (2) Have two quick-closing stop valves installed in the vapor line.

(c) A vapor destruction unit must:

(1) Not be within 30 meters (98.8 ft.) of any tank vessel berth or mooring at the facility;

(2) Have a flame arrester or detonation arrester fitted in the vapor line; and

(3) Alarm and shut down when a flame is detected on the flame arrester or detonation arrester.

(d) When a vapor destruction unit shuts down or has a flame-out condition the vapor destruction unit control system must:

(1) Close the quick-closing stop valves required by paragraph (b)(2) of this section; and

(2) Close the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart.

§154.840 Personnel training.

(a) A person in charge of a transfer operation utilizing a vapor control system must have completed a training program covering the particular system installed at the facility. Training must include drills or demonstrations using the installed vapor control system covering normal operations and emergency procedures.

(b) The training program required by paragraph (a) of this section must cover the following subjects:

- (1) Purpose of a vapor control system;
- (2) Principles of the vapor control system;
- (3) Components of the vapor control system;
- (4) Hazards associated with the vapor control system;
- (5) Coast Guard regulations in this subpart;
- (6) Operating procedures, including:
 - (i) Testing and inspection requirements,
 - (ii) Pre-transfer procedures,
 - (iii) Connection sequence,
 - (iv) Start-up procedures, and
 - (v) Normal operations; and
- (7) Emergency procedures.

§154.850 Operational requirements.

(a) A facility must receive vapors only from a vessel which has its certificate of inspection or certificate of compliance endorsed in accordance with 46 CFR 39.10-13(e).

(b) The following must be performed not more than 24 hours prior to each transfer operation:

(1) All alarms and automatic shutdown systems required by this part must be tested; and

(2) The analyzers required by §154.820(a), §154.824 (d) and (e) of this subpart must be checked for calibration by use of a span gas.

(c) The position of all valves in the vapor line between the vessel's tanks and the facility vapor collection system must be verified prior to the start of the transfer operation.

(d) A tank barge overfill control system that meets the requirements of 46 CFR 39.20-9(b) must not be connected to an overfill sensor circuit that exceeds the system's rated cable length, inductance, and capacitance.

(e) When vapor is being received from a vessel with inerted cargo tanks, the remotely operated cargo vapor shutoff valve required by §154.810(a) of this subpart must not be opened until the pressure at the facility vapor connection exceeds the pressure on the downstream side of the remotely operated cargo vapor shutoff valve.

(f) The initial cargo transfer rate must not exceed the rate agreed upon at the pre-transfer conference required by §156.120(w) of this chapter and 46 CFR 39.30-1(h).

(g) The cargo transfer rate must not exceed the maximum allowable transfer rate as determined by the lesser of the following:

(1) A transfer rate corresponding to the maximum vapor processing rate for the vapor control system, as specified in the facility operations manual required by §154.300 of this chapter; or

(2) The vessel's maximum transfer rate determined in accordance with 46 CFR 39.30-1(d).

(h) While transferring cargo to a vessel connected to a vapor control system, compressed air or gas may be used to clear cargo hoses and loading arms, but must not be used to clear cargo lines.

(i) If one of the two analyzers required by §154.824(d) of this subpart becomes inoperable during a transfer operation, the operation may continue provided the remaining analyzer remains operational; however, no further transfer operations may be started until the inoperable analyzer is replaced or repaired.

(j) Whenever a condition results in a shutdown of the vapor control system, the person in charge shall immediately terminate cargo loading.

(k) If it is suspected that a flare in the vapor control system has had a flare-back, or if a flame is detected on the flame arrester required by §154.828(c)(2) of this subpart, the transfer operation must be stopped and not be restarted until the flame arrester has been inspected and found to be in satisfactory condition.